

REMARKS

The specification has been amended to provide a cross-reference to the previously filed International Application. The specification has also been amended to more clearly explain the purpose of the application and correct typographical errors.

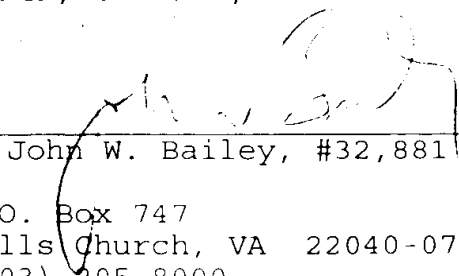
The amendments do not incorporate new matter into the application as originally filed. For example, the amendments at page 24, 34, 66 and 71 simply correct typographical errors. The amendment at page 34 finds support at pages 31-34 of the specification, the amendment at page 66 finds support at page 64, line 11, and the amendment to page 70 finds support at page 34, lines 11-13 of the specification. Entry of the above amendments is earnestly solicited. An early and favorable first action on the merits is earnestly solicited.

Attached hereto is a marked-up version of the changes made to the application by this Amendment.

If necessary, the Commissioner is hereby authorized in this, concurrent, and future replies, to charge payment or credit any overpayment to Deposit Account No. 02-2448 for any additional fees required under 37 C.F.R. § 1.16 or under 37 C.F.R. § 1.17; particularly, extension of time fees.

Respectfully submitted,

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JWB/cgc
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VERSION WITH MARKINGS TO SHOW CHANGES MADE

The paragraph beginning at page 24, line 7 has been amended as follow:

Columns: Shodex OH [pack]pak SB806M (two columns) and
Shodex OH [pack]pak SB802.5 (one column)
(each manufactured and sold by Showa Denko
K.K., Japan):

The paragraph beginning on page 33, line 18 to page 35, line 2 has been amended as follows:

A preferred PTMG used in the present invention as the component (B) has a number average molecular weight of from 500 to 3,000, a molecular weight distribution (Mw/Mn) of 1.75 or less, a content of high molecule weight PTMG molecules of from 2 to 5% by weight, and a heteropolyacid content of from 10 to 900 ppb by weight. Following is a method for producing such a preferred PTMG from THF using a heteropolyacid catalyst. In a reaction system where water is present in an amount sufficient to form a THF organic phase and an aqueous THF/catalyst phase having a specific gravity of from 1.8 to 2.3, the retention time (V/F) of THF is maintained within the range of from 0.5 to 20 hours, preferably from 0.7 to 15 hours. When the V/F value is smaller than the above-mentioned range, the conversion of THF is likely to become

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low. On the other hand, when the V/F value is larger than the above-mentioned range, the reaction time is likely to become long. With respect to the motive power (P/V) applied to the liquid in the reactor, the P/V value is maintained at 1.3 kW/m³ or more, preferably 1.6 kW/m³ or more. When the P/V is smaller than 1.3 kW/m³, the agitation of the reaction system becomes unsatisfactory and the distribution of the diameters of the globules in the reaction system become broad. As a result, the molecular weight distribution of the produced PTMG becomes broad and the control of the molecule weight distribution of the PTMG becomes difficult. By appropriately controlling the V/F and P/V values in the above-mentioned method, it is also possible to obtain a PTMG having a number average molecular weight of more than 3,000 and less than or equal to 4,000, and a content of high molecular weight PTMG molecules of more than 5 % by weight and less than or equal to 10 % by weight.

The paragraph beginning on page 65, line 17 to page 66, line 15 has been amended as follows:

First, a heteropolyacid catalyst solution for use as a polymerization catalyst was produced as follows. A 2-liter reaction vessel was prepared, which is provided with a 3-way cock having three respective ends, wherein each end has attached thereto a condenser and an eggplant type flask for collecting and storing a distillate produced by the condenser, so that the contents of the reaction vessel can be distilled. The thus prepared reaction vessel was used for producing a heteropolyacid

catalyst solution. 1 liter of tetrahydrofuran (THF) and 600 g of silicotungstic acid dodecahydrate were introduced into the reaction vessel in this order, and stirred at 60°C, while continuously removing an azeotropic vapor of water and THF from the reaction vessel. The specific gravity of a solution being formed in the reaction vessel was periodically measured while feeding THF to the reaction vessel every 10 minutes so as to compensate for the total amount of water and THF removed from the reaction vessel. When the specific gravity of the solution became 2.07, the reaction was terminated to thereby obtain a catalyst solution having a specific gravity of [2.01]2.07, namely a solution of heteropolyacid catalyst in a THF/water mixture.

The paragraph being on page 70, line 2 has been amended as follows:

The obtained PTMG (A) had a number average molecular weight (Mn) of 1840, a molecular weight distribution (Mw/Mn) of 1.60, and a content of high molecular weight PTMG molecules which are at least six times as large as the number average molecular weight of all PTMG molecules (hereinafter, simply referred to as "content of high molecular weight PTMG molecules") of 2.29 % by weight. [These values were determined by gel permeation chromatography (GPC) under the conditions mentioned below] The number average molecular weight was determined by the terminal titration method, and the molecular weight distribution and the content of high

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molecular weight PTMG molecules were determined by gel permeation chromatography (GPC) under the conditions mentioned below.

The paragraph beginning at page 71, line 21 has been amended as follows:

Columns: Shodex OH [pack]pak (manufactured and sold by Showa Denko K.K., Japan):
SB 806 M (2 columns)
SB 802.5 (1 column)--

(Rev. 11/13/01)